Unmatched Reliability

Vaughan®

Septage Receiving Inquiry Form

Name: _____
Company: _____
Address: _____
City: _____
State/Country: _____ Zip/Code: _____

Phone: _____
Fax: _____
E-mail: _____
Project Name: _____
Project Location: _____

System:

- ◯ New
- ◯ Replacing

If replacing what is the current issue and what kind of system you are replacing?

_____
_____
_____
_____
_____
_____

Transfer Condition:

Flow_____GPM _____M³/H
TDH_____Feet _____Meters

Application:

- ◯ Transfer
  - ◯ Vertical Wet Well
  - ◯ Submersible
- ◯ Recirculating
  - ◯ Vertical Wet Well
  - ◯ Submersible
- ◯ Mixing

Site Voltage: _____V

Is VFD required?

- ◯ Yes
  - ☐ If yes review with engineering.
- ◯ No

Vaughan requires constant torque VFD

Screening:

- ◯ Screened Solids
- ◯ Filtered Water
- ◯ Un Screened Mixture

Can screens be bypassed?

- ◯ Yes
- ◯ No

Please describe screening system:

_____
_____
_____
_____
_____
_____

Property of Liquids:

Temperature: _____°F _____°C
PH: _____ % SOLIDS: _____
Specific Gravity: _____
Viscosity (cps): _____ (ssu): _____

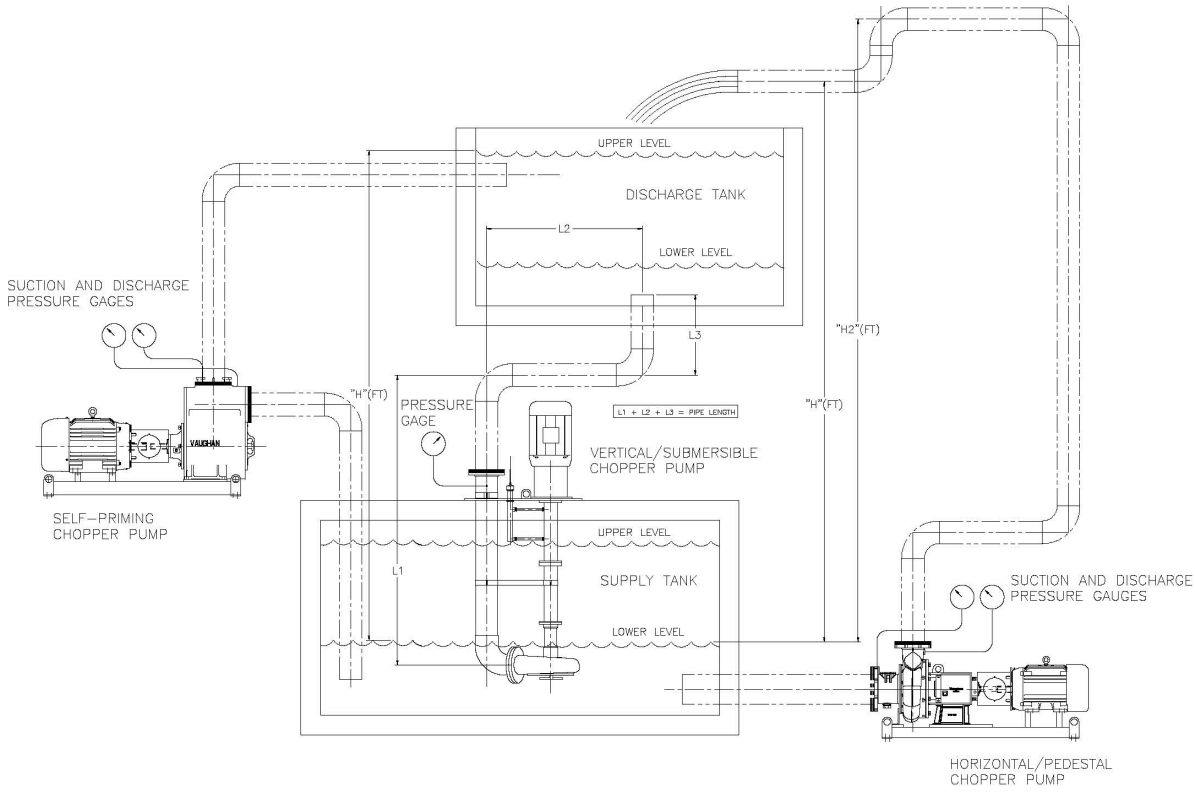
Type of Solids: (check all that apply)

- ◯ Residential Septic Tank Waste
- ◯ Portable Toilet Waste
- ◯ Industrial Waste (specify)
- ◯ FOG/ Grease Trap Waste
- ◯ Other (Specify) _____

_____

Is leaching expected? ◯ Yes ◯ No

TOTAL HEAD CALCULATIONS
CHOPPER



TOTAL HEAD:

TDH = Pipeline Friction + Vertical Lift (H) + Velocity Head ($V^2/2g$)

- Pipeline Friction = [Pipe Length (ft) / 100] x friction factor (table on form V137)

Water friction tables are suitable for sewage & most water-borne slurries up to 5% solids. For high solids loadings & heavy organic sludge, use the biological friction table on form V137.

- Vertical Lift = feet up from supply tank low-water level to high level in discharge tank, or to the center of the open discharge pipe.
  Note: - Lift may be negative (-) if the pipeline is downhill.
  - Intermediate pipeline elevations (H2) higher than the final discharge can be ignored, except that the pump shutoff head must be higher than H2 in order to initiate flow.

- Velocity Head = Energy in the liquid being discharged due to its velocity.
  Note: - Usually ignored as insignificant in low head sump pump systems.
  - For high head systems, use nozzle manufacturer's printed data, or calculate using data as follows:
    V = Velocity of the stream at the discharge diameter (ft/sec)
    G = Acceleration due to gravity (32.2 ft/sec^2)

SPECIAL CASES:

Pipelines with valves & fitting, add appropriate equivalent pipe length.
Pressurized supply or discharge tanks, add the discharge tank pressure, in feet, less any supply tank pressure, in feet, to the above Total Head calculation. Gauge pressure, in psi x 2.31 = head in feet.
Very high solids content sludges & slurries, contact Vaughan on reliable test data for friction values.